



Characterization of Produced Water for Troubleshooting and Facilities Design

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Characterization of Produced Water for Facilities Design and Troubleshooting

- **Issues involved**
- **How to characterize**
- **How to interpret the results**
- **Some examples**

Why Characterize?

- **Regulatory Compliance / Environmental Protection** – to meet quality required by regulatory environment & ultimate fate (disposal, water flood, overboard discharge).
- **Troubleshooting** – characterization provides clues to improving system performance.
- **Design** – a produced water treating system that can handle all types of produced water would be too large and expensive. Successful design is based on the fluid properties to be treated.
- **Contracting & Procurement** – to provide information for equipment suppliers to use to generate proposals and bids.
- **Production Handling Agreements** – to develop realistic specifications for handling production from other owners.

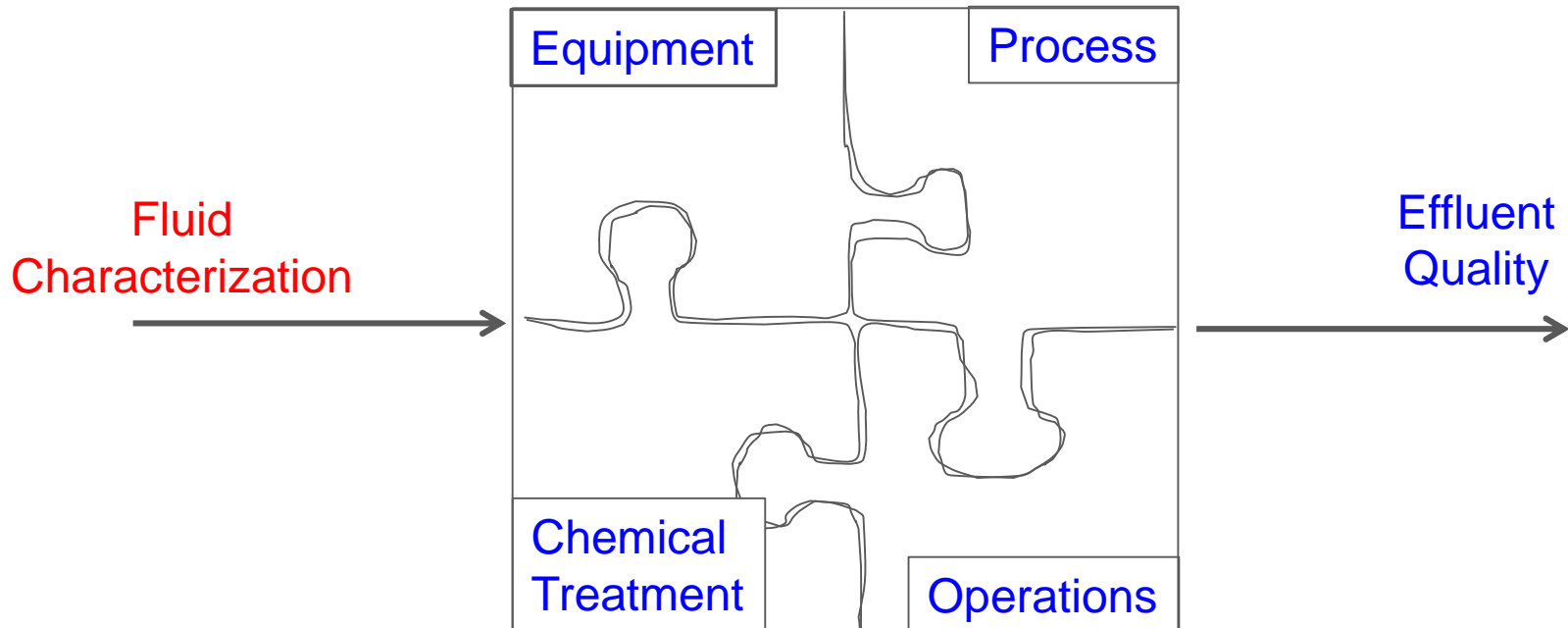
Scope / Role of Characterization

Five Elements in Produced Water System Design and Troubleshooting:

- **Fluid Characterization**
- **Equipment**
- **Process Line-Up**
- **Chemical Treating**
- **Operations**

One key to successful design and effective troubleshooting is to ensure adequate, appropriate, and balanced attention to each of the five elements.

Scope / Role of Characterization



What is produced water?

- **Components Important in Design & Troubleshooting:**

- Dispersed oil
- Dissolved oil (HC, BTX, phenols, PAH, etc)
- Dissolved organic acids (SCFA, VFA, naphthenic acids, PNA)
- Dissolved mineral ions (Na, Cl, Ca, CO_3 , S, Ba, SO_4 , etc)
- Dissolved metal ions (Fe, Zn, Cr, Mn, etc)
- Process & Production chemicals (Cl, MeOH, glycols, LDHI)
- Produced formation solids (clay, sand, carbonate)
- Precipitated mineral solids (CaCO_3 , FeCO_3 , FeS_x , BaSO_4 , etc)
- Precipitated corrosion products (metal oxides)
- Dissolved gases (O_2 , H_2S , CO_2)
- **Combinations of the above (e.g. Schmoo)**
- Various bacteria and by-products (SRB, GHB, etc)

What are the gaps in current practice?

- Need an understanding of what to do with results - what design requirements are implied by any given set of characterization results.
- Interpretation of results is a specialized subject and must be simplified for application by process engineers.
- Need to better understand system performance as a function of fluid characteristics.
- Need a catalog of case studies from which to connect fluid characteristics to the other four elements.

How to Characterize Produced Water

- **Important Analyses in Produced Water Characterization:**
 - **Oil droplet size distribution (on-line and off-line)**
 - **Oil in water concentration**
 - **Oil flow assurance analysis (SARA, wax, paraffin, asphaltenes)**
 - **Gas & oil composition (H₂S, CO₂, BTEX, naphthenates, TAN, biodegradation)**
 - **Water analysis (anions, cations, pH, hardness, alkalinity, dissolved gases , organics, COD, toxicity, etc)**
 - **Scaling tendency & suspended solids concentration, PSD, composition and mineralogy**
 - **Desktop settling, visual observations, and optical microscopy**

How to Interpret the Results

Comparison is the key

Don't evaluate equipment with just a single fluid.

Conversely: don't expect equipment to work for all fluid types

Evaluate equipment using several fluid types in order to establish an "operating envelope"

Compare the fluid of interest against Industry Benchmark fluids

Compare the fluid of interest against other fluids in the region

Develop a catalog of fluid characteristics and the systems that work for those fluids (equipment, process, chemical treating, operations).

Typical Oil vs Gas Produced Water Properties:

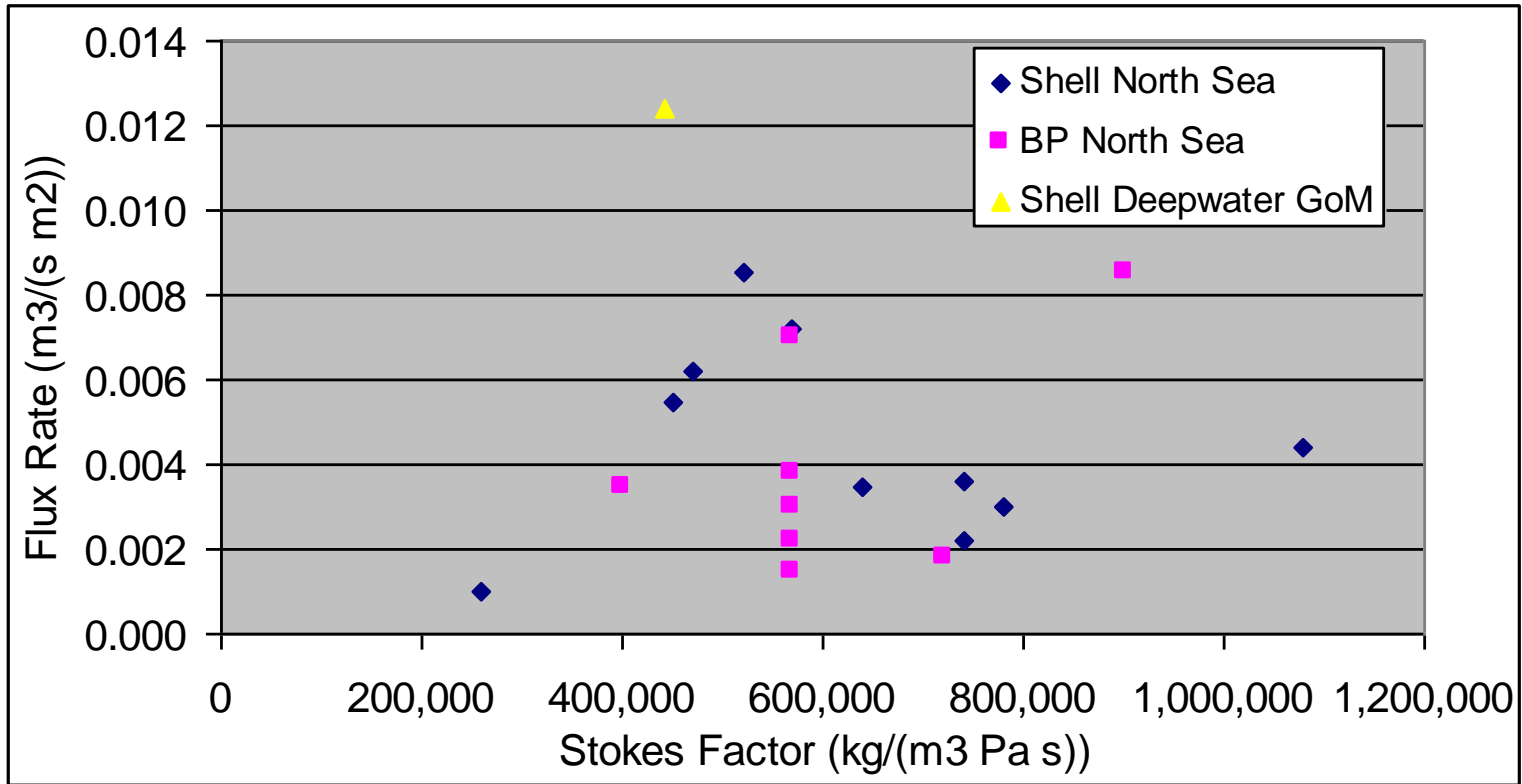
Table 2.1
Typical hydrocarbon discharges from a selection of
North Sea oil and gas production platforms (1989)

		Oil platforms	Gas platforms
Number of platforms measured		12	15
Total oil or gas production	sm ³ /d	75,600 (475,500 bopd)	49,100,000 (1,734 MMscfd)
Total produced water	m ³ /d	63,713	612
Total hydrocarbon discharge [1]	tonne/y	500	216
Dispersed oil concentration	mg/l	15.3	483.9
Dissolved oil concentration	mg/l	6.2	481.9
Polar hydrocarbon concentration	mg/l	165.9	230.1

[1] Refers to mineral hydrocarbons e.g. aliphatic and aromatics, does not include polar hydrocarbons such as organic acids.

Source: "The composition of produced water from Shell operated oil and gas production in the North Sea", International Produced Water Symposium, Feb. 1992, San Diego, submitted by SIPM/Expro/NAM, ref 1.01.1.b.

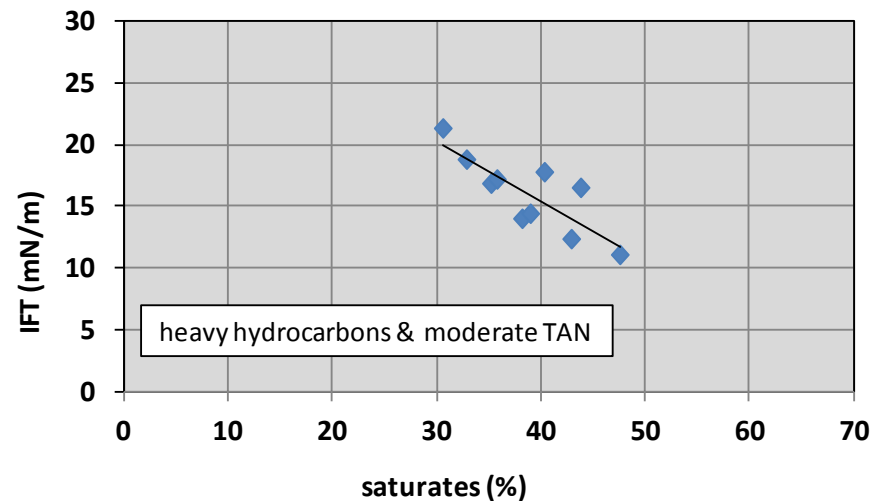
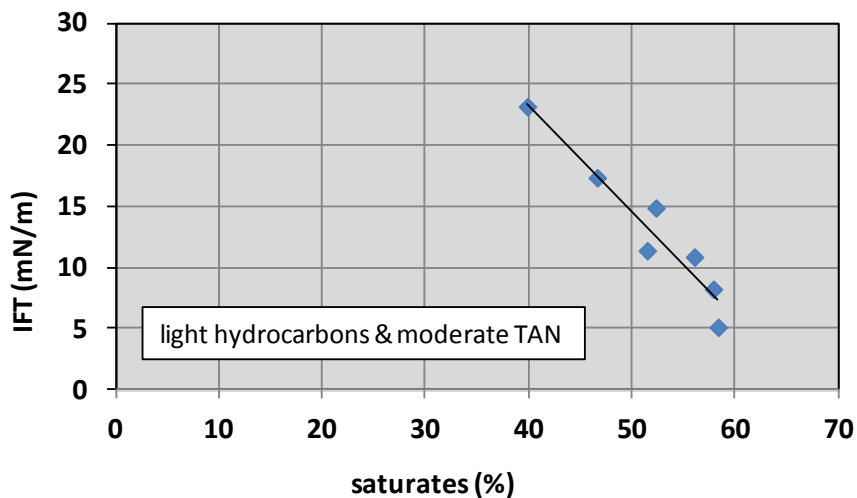
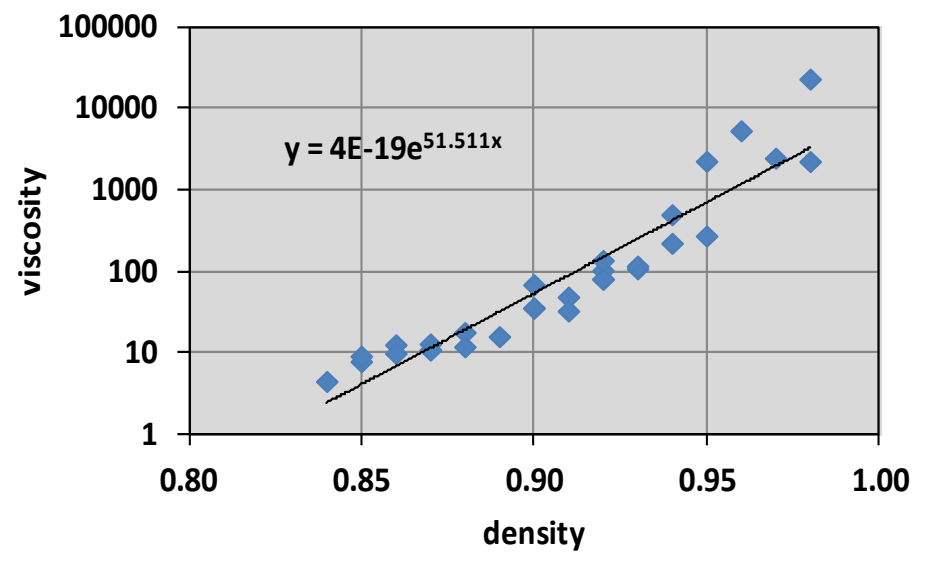
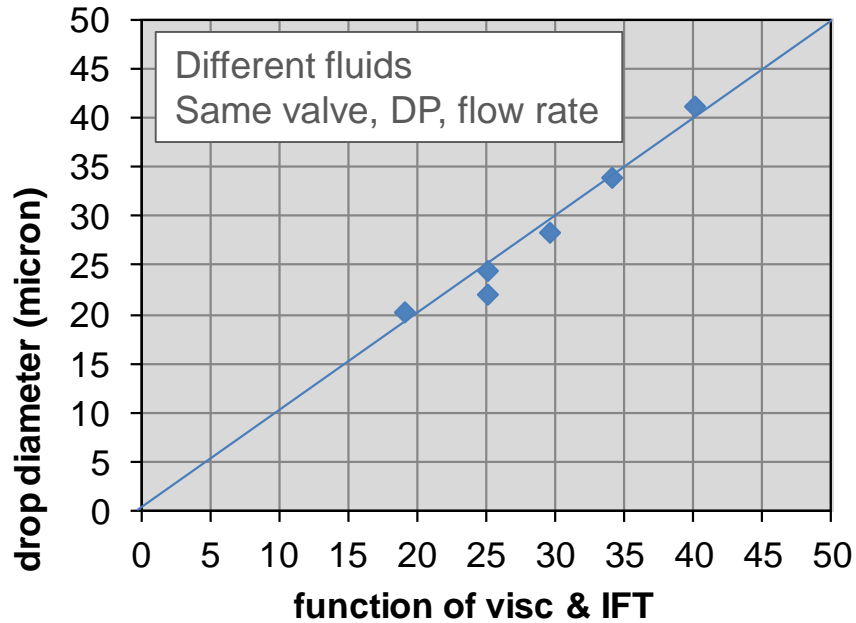
Simple Characterization – Stokes Factor



Stokes Factor:
$$S = \frac{\rho_w - \rho_o}{\mu_w}$$

Deepwater – high cost of space and weight in deepwater resulted in high flux rates

Fluid Property Database as part of Drop Size Estimation



Characterization Example – Deepwater USA

Next Several Slides:

- **Characterization of produced water for: Deepwater Offshore USA**
- **Characterization for a particular project should include a comparison with nearby projects, particularly if similar or analogous equipment is planned to be used**
- **Subsurface setting (depth, T, geochemistry, salt deposits, fines)
Possibility of biodegradation**

Water Characterization Deepwater USA

Oil

- **Mostly Miocene age fluids, API: 24 to 40, mostly 27**
- **Mostly deep: 3,500 to 5,500 meters**
 - **Reservoir T: 54 to 80 C**
- **A few waxy wells**
- **Resins & Asphaltenes not a down hole problem, but is a topsides problem: O/W & W/O emulsions**
- **Biodegradation, acids, and naphthenates in a few wells**

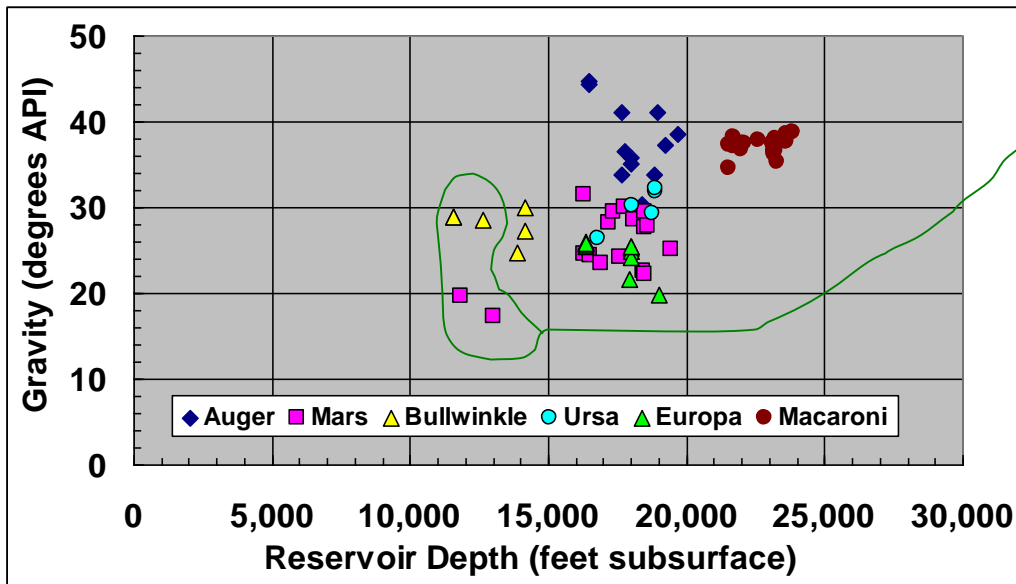
Water

- **Sweet / 0.2 mole % CO₂ / pH around 5.5**
- **Salt domes: 20 to 24 % salt & Barium: 120 to 260 mg / L**

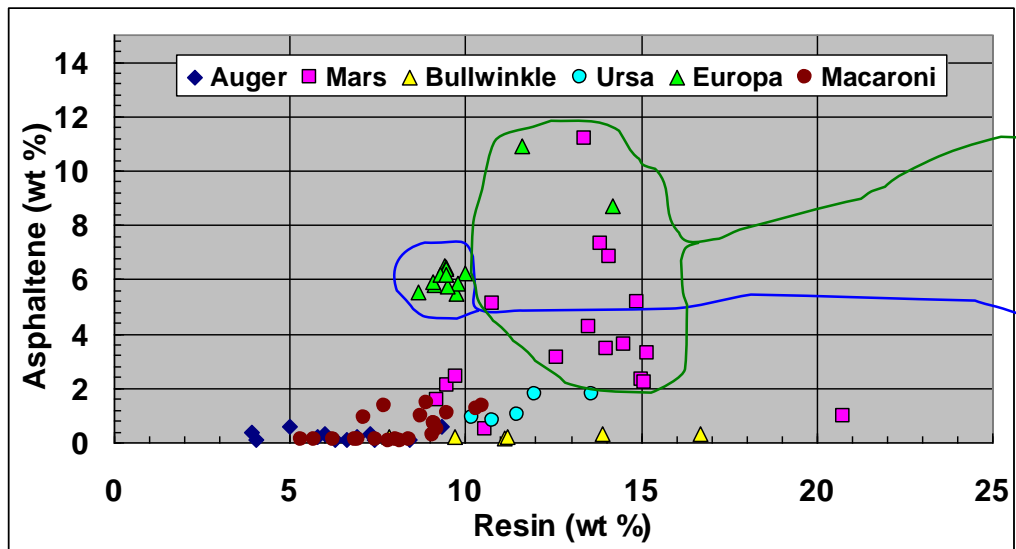
Solids

- **Solids:**
 - **Fines from unconsolidated sands & scale precipitation**
 - **ASTM D-4807: low to 150 to 250 lbs / MBbl**

Subsurface setting & Oil characterization by asset & by region



Biodegradation ceiling around 13,00 ft. Confirmed biodegradation for 2 Mars and 2 Bullwinkle wells - made water treating more difficult. Low API and high Total Acid Number (TAN) are indicative of biodegradation.



High resin + asphaltene content for several wells on Mars and Europa - makes water treating more difficult.

High asphaltene w/o high resin makes water treating even more difficult.

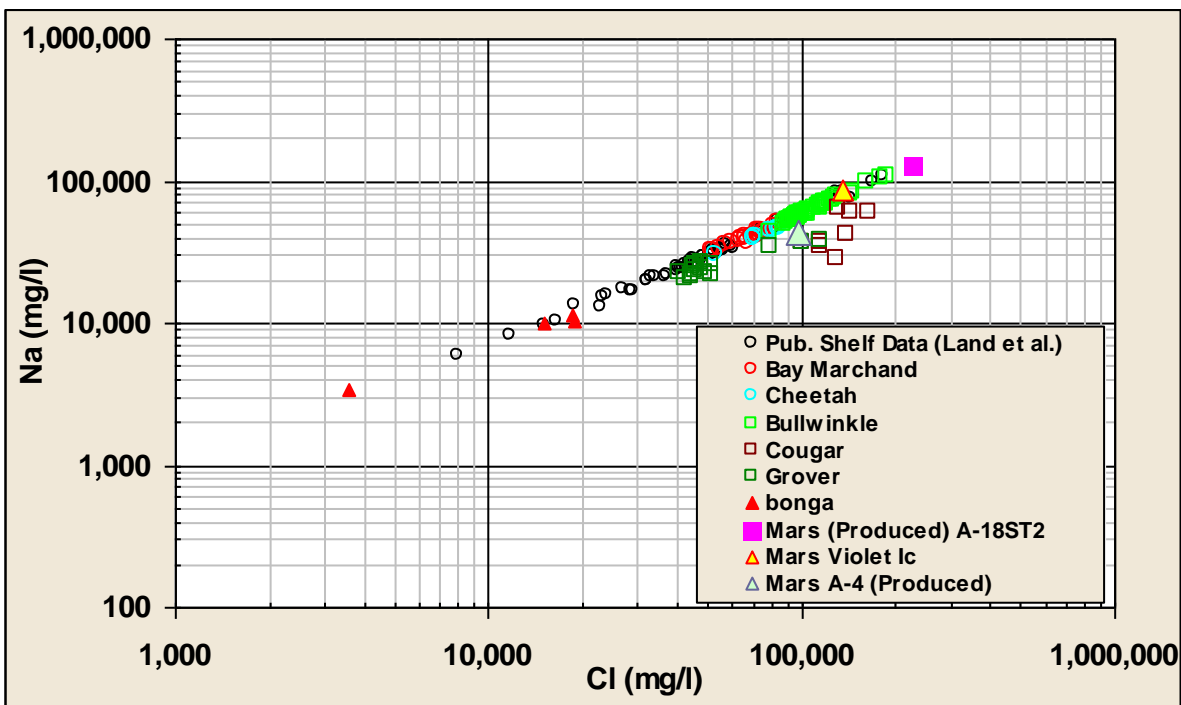
Mars Platform Oil Characterization

Reservoir	DEPTH	API	Saturates	Aromatics	Resins	Asphaltenes	Atomic S (wt %)	ACID No.
Pink	13,036	17.3	21.0	61.6	14.0	3.4	2.7	4.35
Lower Green	16,287	31.5	40.9	47.6	9.5	2.1	1.8	0.34
Ultra Blue	16,301	24.6	41.3	37.5	13.9	7.3	2.6	
Orange	16,550	24.4	27.4	54.5	14.5	3.6	2.4	1.00
Upper Green	16,910	23.5	24.3	55.6	14.9	5.2	2.6	
Magenta	17,610	24.2	28.1	54.1	13.5	4.3	2.6	0.61
Violet Ic	18,419	22.5	25.0	59.3	12.6	3.1	2.7	1.20
Lower Yellow	18,476	27.6	30.8	51.8	15.1	2.2	2.2	
Terra Cotta	18,476	22.1	25.2	50.2	13.4	11.2	2.8	0.95

Partial characterization of hydrocarbons for Mars TLP.

Shallow reservoir (Pink) above biodegradation ceiling – severe biodegradation.

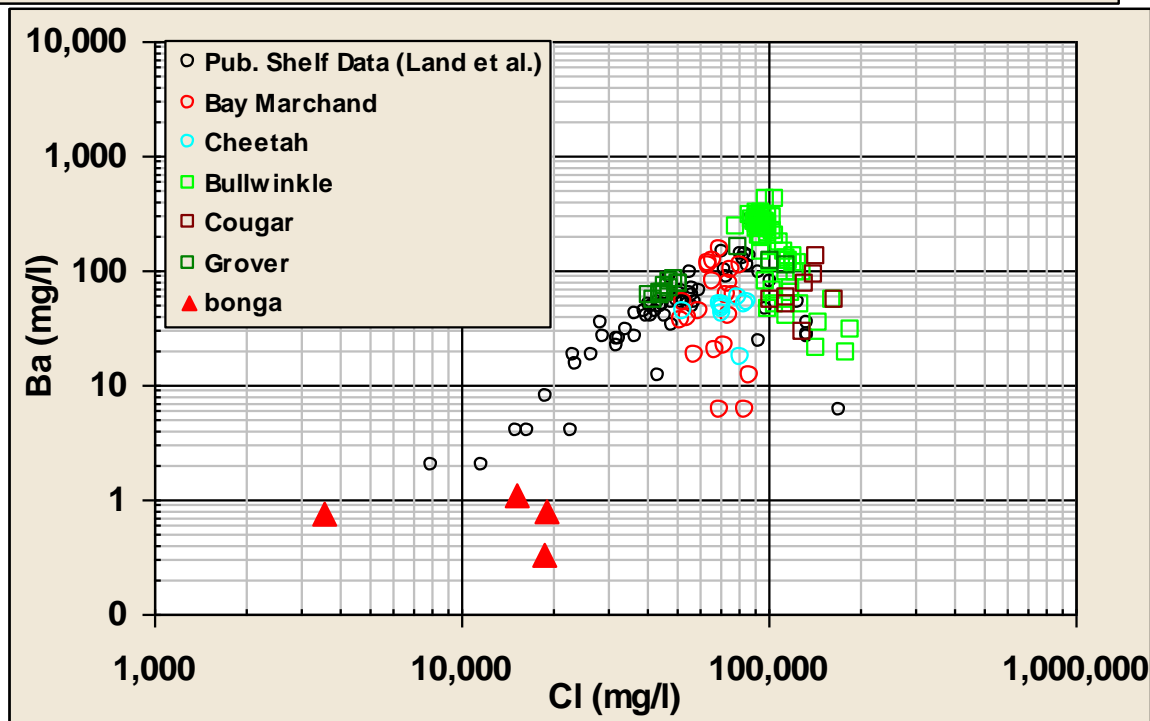
Moderate API but asphaltenes + resins are high. Given high aromatic & resin concentration, asphaltenes likely to be relatively stable. However, risk of incompatibility with high API fluids from subsea systems through satellite hub concept.



Water chemistry for various shelf and deepwater locations.

As shown, both shelf and deepwater locations have high salinities.

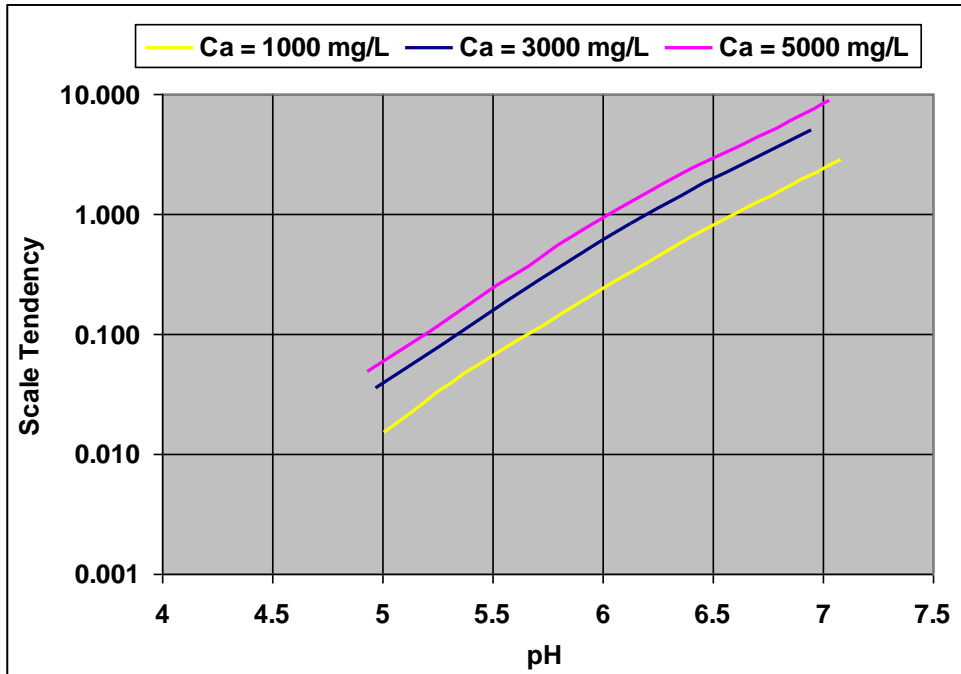
Deepwater water chemistry analogous to shelf - not a step-out.



High salinity gives a high density difference - good for water treating.

Scaling components present. Scale analysis required.

Scale Tendency Analysis



Calcium carbonate scale is common in E&P. Calcium comes from the formation water. Carbonate comes from dissolved CO₂, and from bicarbonate in the formation water.

Scale Tendency > 1: thermodynamic possibility of scale formation.
Scale Tendency > 3: mandatory within Shell to mitigate scaling with scale inhibitor.

Specific Water Chemistry – Mars TLP

Specific Gravity	1.125
pH	6.5
Cations	mg/L
Sodium	61,321
Calcium	5400
Magnesium	1626
Barium	159
Iron	20
Anions	mg/L
Chloride	109,000
Bicarbonate	122
Sulfate	1
Total Dissolved Solids (TDS)	177,643

Gas phase: no H₂S, only 0.1 mol % CO₂

High calcium, high magnesium, moderate bicarbonate, low CO₂ in the gas, no H₂S therefore no alkaline scavengers → no calcium carbonate or magnesium carbonate scaling.

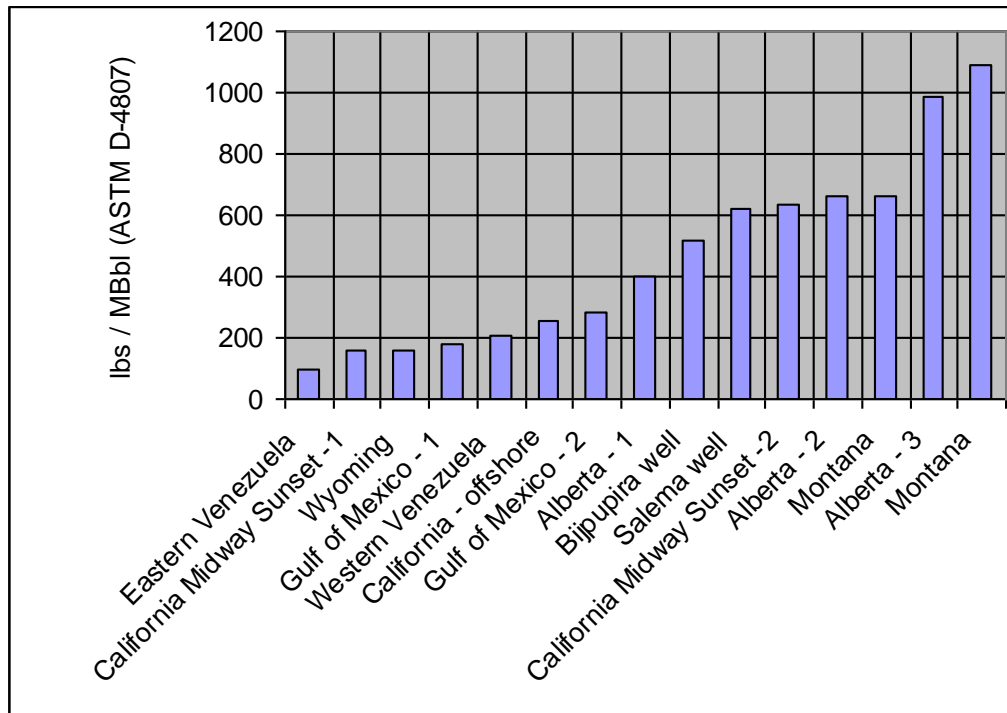
Iron relatively high but no H₂S so no iron sulfides.

High barium, and some sulfate, high salinity so barium sulfate relatively stable.

Solids Characterization

- Solids measured using ASTM D-4807, with 0.45 micron filter.
- Results reported as lbs/MBbl.
- High solids levels are likely to cause tight solids-stabilized emulsions.

Proper solids characterization should include mass, size distribution, wetting properties (oil or water), composition.



Solids content of three Shell deepwater facilities compared to global benchmark high solids crude oils - high solids makes water treating very difficult.

Bullwinkle Solids Analysis:

Deionized Water Wash*	<u>19.7%</u>	
(*Includes substances soluble in water such as salts)		
Xylene Wash*	<u>9.6%</u>	
(*Includes substances soluble in xylene such as paraffin, oil, and organics)		
Acetic Acid Wash*	<u>27.7%</u>	(Iron Carbonate <u>Pos</u>)
(*Includes substances soluble in dilute acetic acid such as carbonate scale)		
Hydrochloric Acid Wash*	<u>27.4%</u>	(Iron Sulfide <u>Pos</u>)
(*Includes substances soluble in 15% HCl acid such as iron sulfide or iron oxide)		
Acid Insolubles*	<u>15.6%</u>	
(*Includes substances insoluble in 15% HCl acid such as sulfate scale, sand, & s		



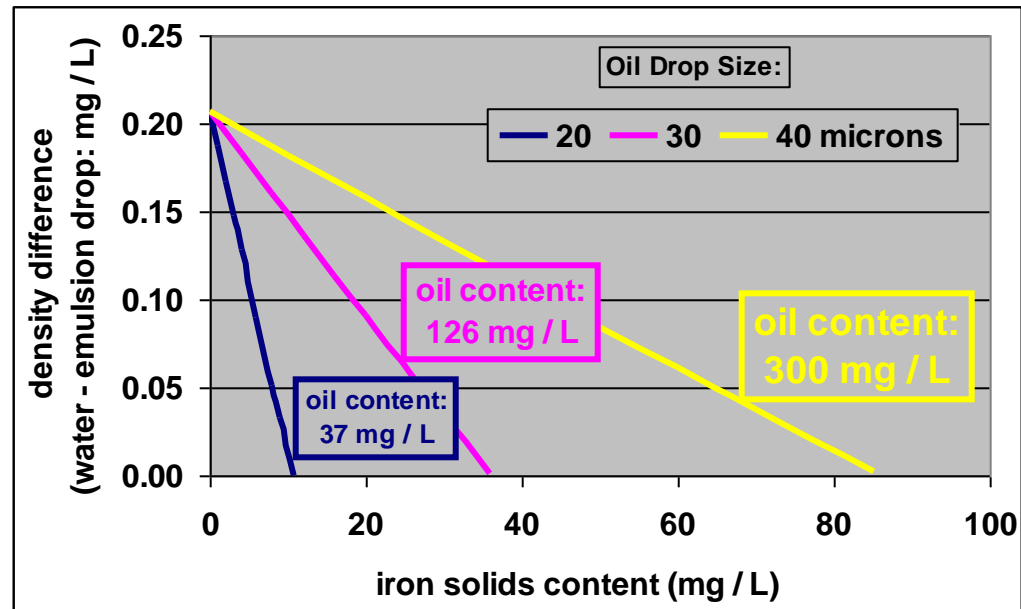
20 % salts
10 % waxes, asphaltenes
28 % carbonate scale
27 % iron compounds
16 % sulfate scale & silica fines

Oil/solids conglomerate are typically a mixture of sticky nasty things

Fine solid particles add stability to oil in water emulsions

Solids also increase the density of the oil drop

When oil drops plus solids are neutrally buoyant they cannot be separated by settling or hydrocyclones



What was learned from Deepwater US characterization:

Characterization of produced water for: Deepwater Offshore United States

Example of all the information that goes into a proper characterization of produced water

- | | |
|---|--|
| Subsurface setting (depth, T, geochemistry, salt deposits) | High salinity seen across the region which gave high density differences, some scale problems addressed with SI, required separate trains to segregate incompatible fluids. |
| Possibility of biodegradation | Handful of wells caused havoc. Extensive vessel internals modifications, process re-routing and chemical treatment work. |
| Gas constituents (CO ₂ , H ₂ S) & process conditions (T, P) | CO ₂ / carbonate equilibria required scale inhibitor at DP locations, but not severe. |
| Oil characterization | Resins and asphaltenes caused foaming, emulsion, and PWT problems. Had to apply special chemistries, keep PWT equipment clean, develop special acid flow back procedures, change process routing, minimize recycles, avoid condensate mixing w/ oily water, minimize shearing, improve treatment of recycle streams. |
| Brine analysis by asset & by region | High iron was used to advantage w / DTC chemistry. |
| Possible solids from reservoir | Cleaned vessels frequently. Auger applied an acid treatment. Solids wetting demulsifiers applied at Mars. |

Most Difficult Characteristics of Produced Water:

Worst Characteristics of Produced Water:

- **Solids (in general) and Iron Sulfides (in particular):**
 - Water wet or Oil Wet?
 - Buoyancy of Conglomerate (oily solids)?
 - Organic or Inorganic?
 - Particle size distribution?
 - Source? (often eliminating the source is the best treatment strategy)

- **Biodegradation:**
 - High acid concentration?
 - Calcium naphthenate?

- **Unstable asphaltenes:**
 - SARA analysis (& stability plot – to be discussed)

- **Production Chemicals:**
 - Methanol, AA Hydrate Inhibitors, Corrosion Inhibitors?
 - Over-dosing?

Characteristic	Source	Design Detail	Possible Points	Characteristic	Ranking Points
Stokes Factor	API, temperature, water density	Longer residence time in primary separators	10	< 200,000	10
				400,000 to 800,000	5
				> 800,000	0
Oil flow assurance factors	Wax, paraffin, asphaltene stability, incompatible hydrocarbons	Inhibitors, heating for wax and paraffin	5	No inhibitors or heating required	2
				Inhibitor or heating required and none used	5
				Inhibitor or heating required and is used	0
Biodegradation	TAN, fingerprinting, biomarkers	Secondary separation equipment, optimized chemical treatment	15	0 wells	0
				1 to 2 wells Delta API > 2	10
				> 2 wells Delta API > 2	15
Scaling tendency	Mineral scales e.g. carbonates, sulfates; incompatible water	Water wetting chemicals, filtration / tertiary separation equipment	5	No inhibitors required, or inhibitor required and is used	0
				Inhibitor required and none used	5
Dissolved organics	Acids, naphthenates	Secondary separation equipment, optimized chemical treatment	5	pH > 6, acid < 100 mg/L	0
				4 < pH < 6 100 < acid < 500	3
				pH < 5 acid > 500 mg/L	5
Solids	Formation fines, scale particles,	Water wetting chemicals, filtration / tertiary separation equipment	15	Solids < 100 lb/MBbl	0
				100 < solids < 400	10
				Solids > 400 lb/MBbl	15
Iron sulfide	H ₂ S, iron	Secondary separation equipment, optimized chemical treatment	20	FeSx < 10 mg/L	15
				10 < FeSx < 50	18
Surface active or shear enhancing chemicals	Corrosion inhibitor, methanol	Secondary separation equipment, optimized chemical treatment	10	No change upon turning off chemical	0
				Moderate water deterioration w/chemical	5
				Severe water quality deterioration w/ chemical	10
Small drops	High shear	Reduce shearing	15	D < 10 micron	15
				10 < D < 50	10
				D > 50 micron	0

Type 1 System: Total points less than 35

No iron sulfide. No biodegradation.

A typical system may consist of primary separation followed by hydrocyclones. Flotation may be required, depending on the Stokes Factor. See the example below.

Type 2a System: Total points between 35 and 55

No iron sulfide. No biodegradation.

A typical system may consist of primary separation, hydrocyclones and flotation. Care should be given to the handling of reject streams from the water treating equipment in order to ensure that a stabilized emulsion is not generated.

Type 2b System: Total points between 35 and 55

Presence of iron sulfide or biodegradation.

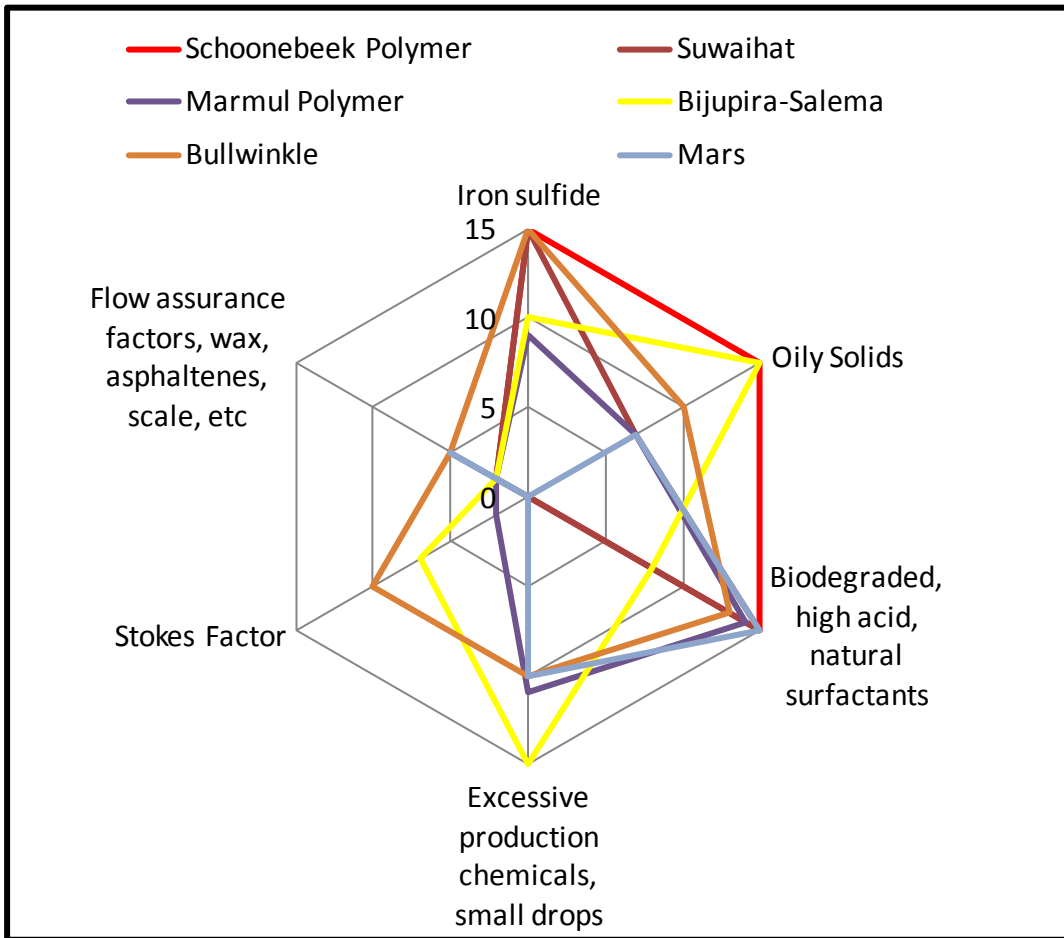
For this level of separation challenge, a typical system may consist of primary separation, hydrocyclones, flotation and some means of treating the reject from the water treating equipment. Chemical application will be critical both in terms of demulsifier and deoiler selection and optimization, but also in terms of minimizing the use of methanol and corrosion inhibitor.

Type 3 System: Total points above 55

Presence of iron sulfide and / or biodegradation.

A typical system may consist of primary separation, hydrocyclones, flotation and some means of treating the reject from the water treating equipment. Chemical application will be critical both in terms of demulsifier and deoiler selection and optimization, but also in terms of minimizing the use of methanol and corrosion inhibitor. Some form of tertiary water treating equipment will be required such as filtration, or centrifugation.

Catalog of Fluid Types



This is a collection of problematic produced waters.

For each fluid, a successful produced water treating system (equipment, process, chemicals, operations) has been identified

How to Characterize Produced Water

- Oil droplet size distribution
- Oil in water concentration
- Oil flow assurance analysis
- Gas & oil composition
- Water analysis
- Suspended solids concentration, PSD, composition and mineralogy
- Desktop settling, visual observations, and optical microscopy

